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BOILING OF NITROGEN AT VARIOUS PRESSURES WITH

NONSTATIONARY HEAT INPUT

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Liquid-nitrogen boiling times have been measured at 0.1, 1.3, and 2 MPa by means of a piezoelectric sensor; there is a relationship to the homogeneous nucleation temperature.

The discovery of high-temperature superconductivity has raised interest in research on heat transfer in liquid nitrogen. We have measured the boiling times  $t_A$  for liquid nitrogen on step heat input, which simulates the transition to the resistive state in a current-carrying superconductor film on a substrate, where we examined the effects of pressures up to 2 MPa.

The apparatus, including the heater and the boiling recorder, has been described [1]. There was also a pressure-measurement system containing a high-pressure cell made of copper and a Sapfir pressure sensor, together with a thermometer. The cell was placed in liquid nitrogen at atmospheric pressure, i.e., all the measurements were made at 77.4 K. Figure 1 shows the results, where the solid lines correspond to the calculation described in [1]. A step-heated liquid in contact with a fast heater boils in accordance with

$$q \sqrt{t_{\rm A}} = A \Delta T_*, \tag{1}$$

in which

$$A = \frac{\sqrt{\pi}}{2} \left( \sqrt{\lambda C \rho}_{\ell} + \sqrt{\lambda C \rho}_{\mathbf{s}} \right);$$

where  $\rho$  is density, C is specific heat,  $\lambda$  is thermal conductivity, and  $\Delta T_{\star}$  is the limiting attainable superheating for a given liquid at the corresponding pressure. The subscripts  $\ell$  and s relate to the liquid and substrate. The temperature is taken as the average of  $T_0 = 77.4$  K and the value  $T_{\star}$  corresponding to the pressure in the cell, the limiting attainable temperature, which has been calculated for example in [2].

The pressure was limited to 2 MPa, although the critical pressure for nitrogen is  $P_{\rm Cr} \approx 3$  MPa, because of the physically obvious reduction in the sensor signal on boiling as the pressure increases, i.e., as the critical point is approached. That reduction can be estimated from the [3] model: explosive growth of a vapor bubble produces an amplitude in the pressure wave  $\Delta p \sim (\rho_{\ell} - \rho_{V}) (dR/dt)^{2}$ , in which R is radius and  $\rho_{V}$  the vapor density. The growth rate is

$$\frac{dR}{dt} \sim \frac{q \, \sqrt{(\lambda C \rho) \, \varrho}}{A \rho_{\rm v} \, L},$$

in which L is the latent heat of evaporation. The numerical values give  $\Delta p_{0.1}/\Delta p_2$  as 300, while the ratio of the signal amplitudes at 0.1 and 2 MPa was 100, i.e., the values agree as to order of magnitude.

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Fig. 1. Nitrogen boiling times  $t_A$  in sec in relation to heat flux density q at the heater in  $10^4$  W/m<sup>2</sup> at pressures in Mpa of: 1) 0.1; 2) 1.3; 3) 2.

TABLE 1. Limiting Superheating Temperatures

Pressure, MPa	$q V \overline{t_A},$ W·sec <sup>1/2</sup> ·cm <sup>-2</sup>	Т <sub>*е,</sub> қ	<i>т</i> <sub>*С, К</sub>
0,1	2,86	$108,5\pm0,7$	111
1,31	3,37	$115,8\pm1,1$	116
2,0	3,69	$120,1\pm1,2$	119

Table 1 gives the limiting attainable superheating  $T_{*e}$  from (1) via the measured  $t_A$  and the value calculated,  $T_{*c}$ , from homogeneous nucleation theory.

The conclusions are as follows:

1. To estimate the boiling time with a fast film heater, one can use (1) with the constants corresponding to the average of  $T_0$  and  $T_{\star}$  for the corresponding pressure, where the estimation accuracy is evident from Fig. 1 (Table 1 gives the standard errors).

2. Raising the pressure to 2 MPa increases  $t_A$  by a factor of 1.7, which can be used to improve the stability and reliability in the corresponding devices.

## NOTATION

 $\Delta p$ , pressure step on boiling;  $\pi = 3.14...i \Delta p_{0.1}$ ;  $\Delta p_2$ , pressure steps at pressures in cell of 0.1 and 2 MPa correspondingly;  $t_A$ , boiling delay from start of heating to appearance of sensor signal; q, heat flux density at heater;  $T_0$  and  $T_*$ , bath temperature and limiting superheating.

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